

REINHOLD ENVIRONMENTAL Ltd.



2016 APC-Wastewater Round Table & Expo Presentation

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Flexibility of RSC²[™] Design to Accommodate Various Processes & Waste Streams

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Outline

- ▶ Regulatory Overview
- ▶ A-S-H[®] RSC^{2™} Remote Submerged Chain Conveyor
- ▶ How RSC^{2™} Accommodates Closed Loop Flow
- ▶ System Water Balance & Plant Wide Water Management
- ▶ Water Quality Considerations
- ▶ RSC^{2™} Module Approach for Advanced Treatment

ELG (for units > 50 MW)

Waste Streams	Technology Basis
FGD Wastewater	Chemical Precipitation + Biological Treatment
Fly Ash Transport Water	Dry Handling
Bottom Ash Transport Water	Dry Handling/Closed Loop
FGMC Wastewater	Dry Handling
Gasification Wastewater	Evaporation
Combustion Residual Leachate	Impoundment
Nonchemical Metal Cleaning Waste	[Reserved]

What Water Applies to ELG?

▶ Includes

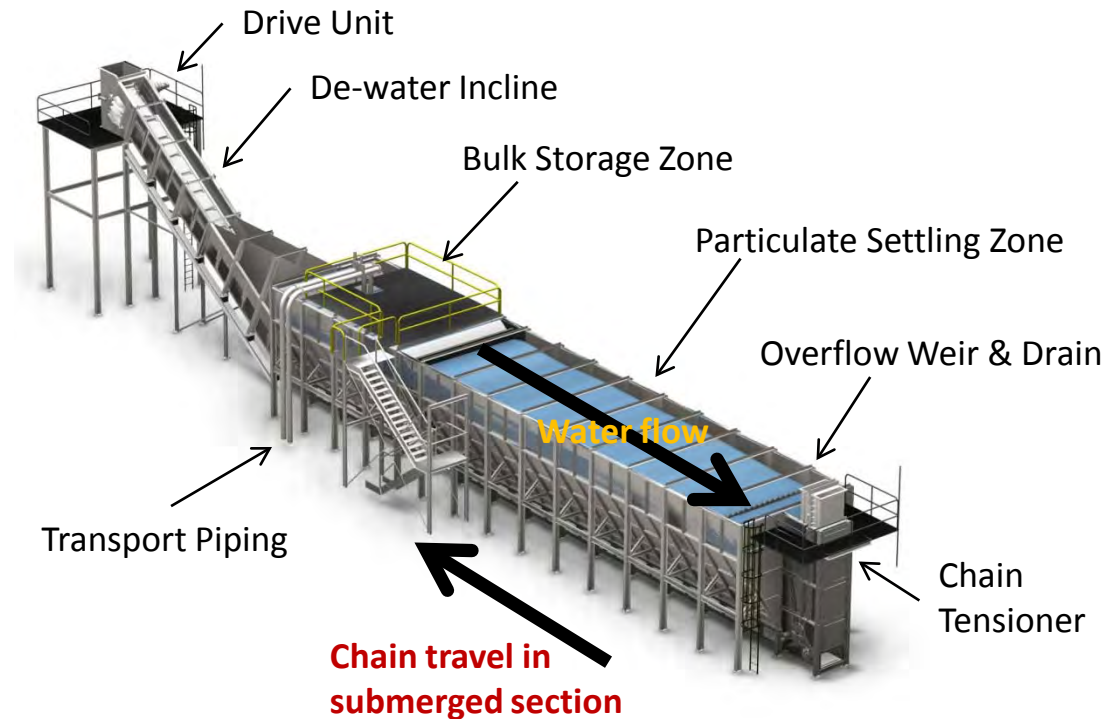
- Transport water (bottom ash and economizer)
 - 1,500 – 3,500 GPM/line
- Water from draining a wet sluicing containment vessel
 - 100,000 – 500,000 Gallons

▶ Excludes

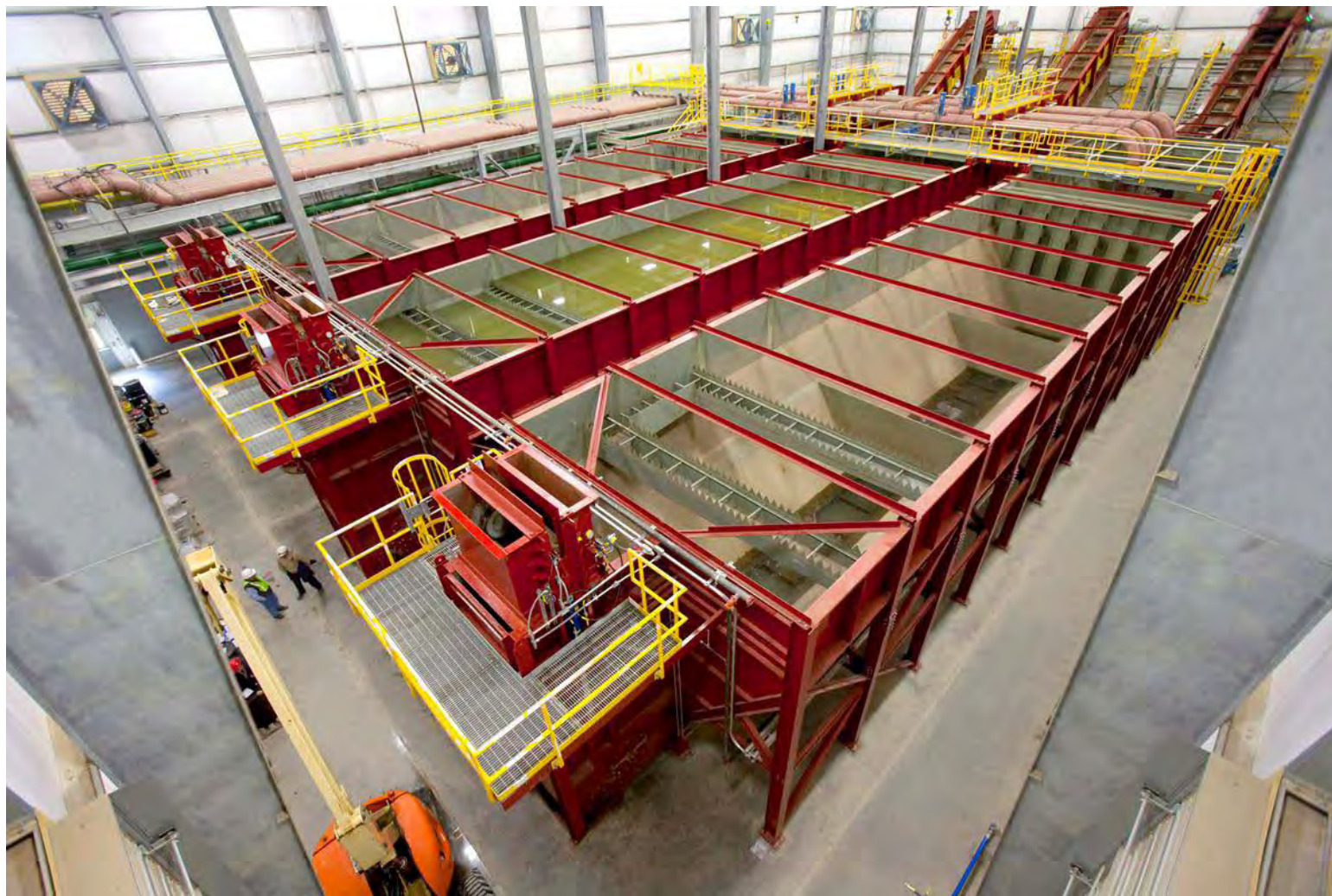
- Quench water (ash hopper service water)
 - 300 – 500 GPM/unit
 - Note quench water becomes transport water in wet sluicing systems
- Discharges from minor maintenance events
 - Valve leaks, minor line leaks, grinder or pump seal failures, etc.

A-S-H[®] RSC^{2™} Remote Submerged Chain Conveyor

- Located remote from boiler area
- Usually can keep existing sluice system as-is
 - Minimal outage time for installation
- Dewater ash to landfill-able moisture content
- Clarifies transport water



(3) 50% Capacity RSC²™ Units for (4) Boilers

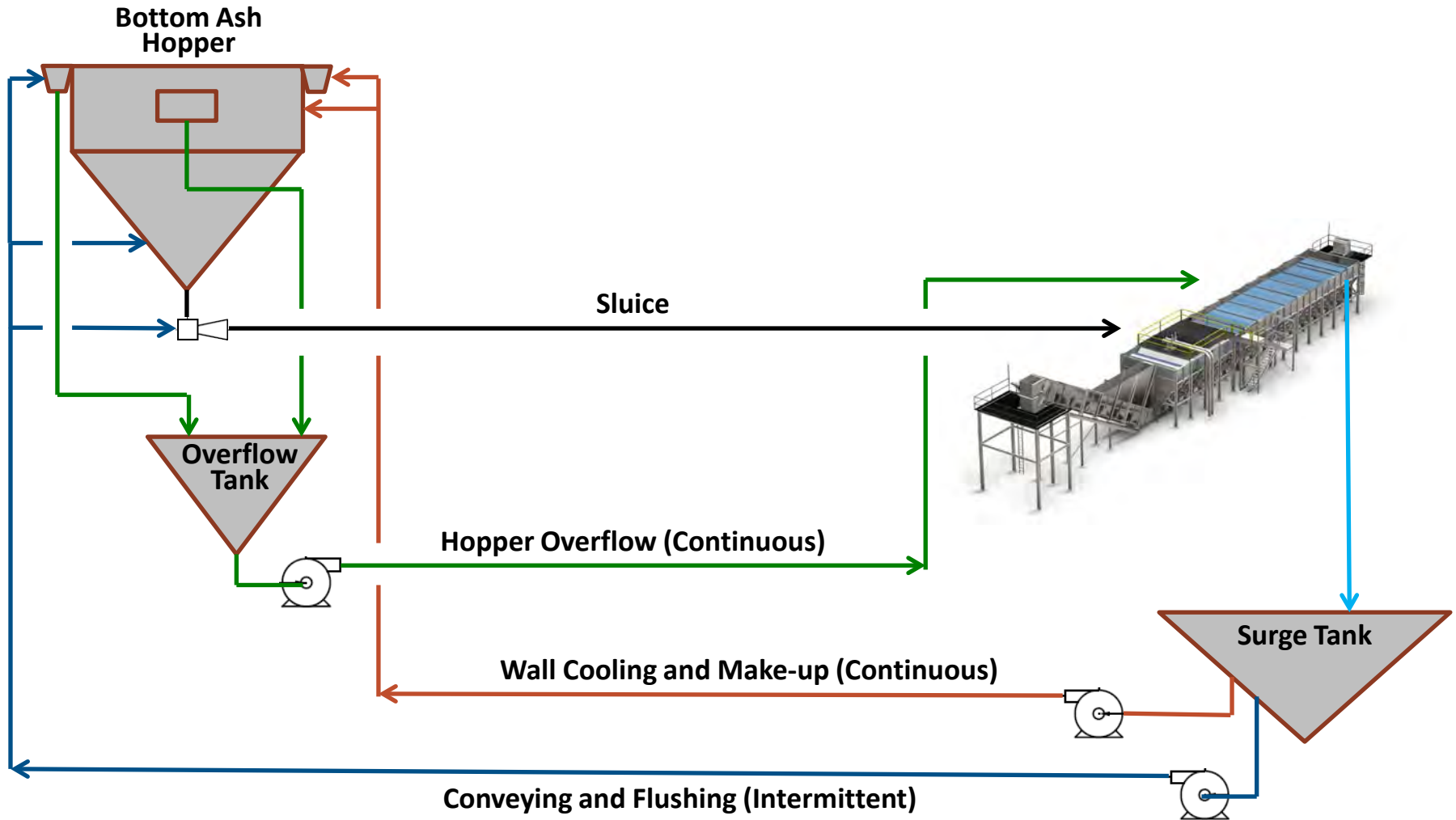




Dewatered Ash Pile



How RSC²™ Accommodates Closed Loop Flow



Surge Tank

- ▶ Surge tank manages water inventory in system
- ▶ Minimum volume required for recirculating pump suction
- ▶ Capacity to drain system volumes
 - RSC2™ volumes
 - Ash hopper volumes
 - Piping volumes
 - Overflow tanks

System Water Balance

- ▶ Water losses
 - Ash hopper evaporation (5 – 15 GPM/unit)
 - Retained moisture in dewatered ash (2 – 20 GPM/unit)
 - Hopper leakage?
 - Natural evaporation (<1 GPM yearly average)
- ▶ Water additions
 - Seal water for pumps (20 – 100 GPM total for all pumps in system)
 - Rain if not in building (<1 GPM yearly average)
- ▶ Need to ensure net loss of water in system
 - Helps control water chemistry
 - Consider mechanical pump seals
 - Ways to get rid of water from system?

Plant-Wide Water Management

- ▶ Ways to get rid of ash transport water
 - Makeup to FGD
 - Consider water quality requirements
 - Fly ash conditioning

- ▶ Other ways to use closed loop ash system
 - Non-chemical metal cleaning wastes with significant solids content
 - Boiler wash
 - Air pre-heater wash
 - Precipitator wash
 - ELG would not allow ash transport water to go to low volume waste pond after being used in another process

Reuse of Ash Transport Water to FGD Systems

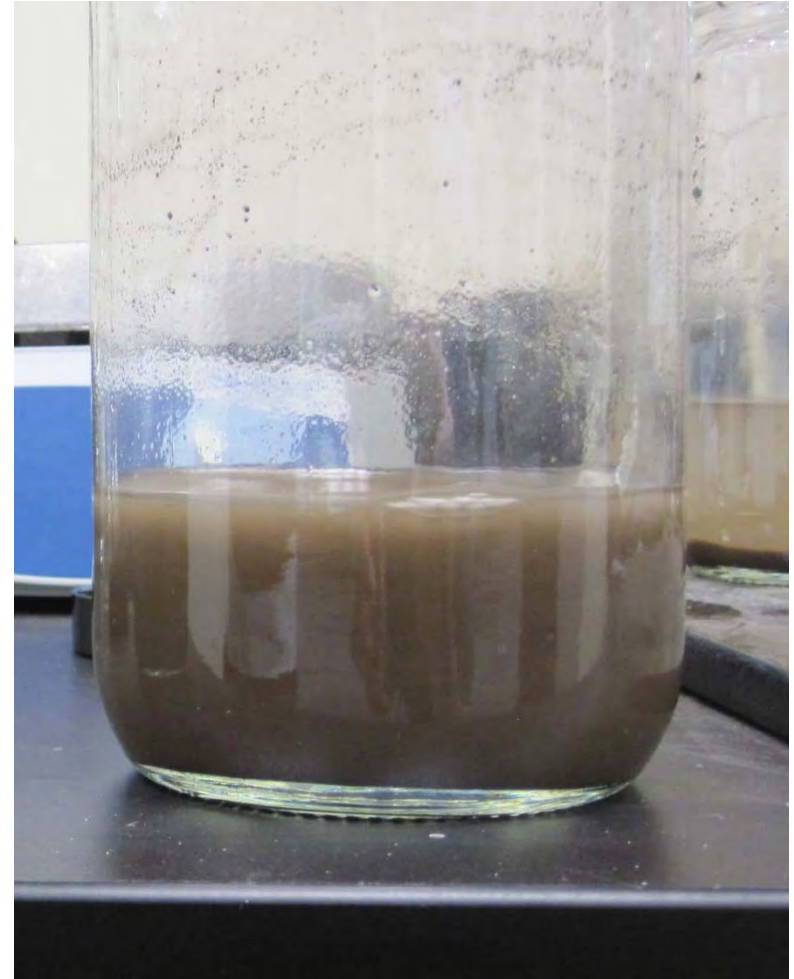
- ▶ Ash transport water generally has low TDS, which makes it suitable for FGD makeup
 - Some coal sources may require scale control measures in the bottom ash system. These measures should be evaluated for impact to FGD.
- ▶ Need to ensure low TSS (<100 ppm)
- ▶ Possible impacts of poor makeup water quality are:
 - Lowered gypsum purity
 - Altered gypsum morphology
 - Lowered limestone dissolution
 - Mist eliminator scaling
 - Increased metals of concern in the system effluent

Equipment Wash-down Water

- ▶ Not necessarily required to be closed loop but RSC²[™] can be used to treat and re-use this water
 - Boiler wash
 - Air pre-heater wash
 - Precipitator wash
- ▶ Water quality
 - Typically high in fines content
 - Can be very low pH (pH = 2)
- ▶ Fines can be captured in RSC²[™] with advanced treatment modules
- ▶ Consider dewatered moisture content
 - Fine ash will require longer dewatering time in bunkers than bottom ash

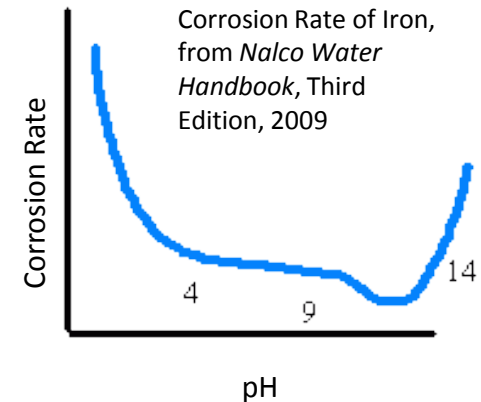
Water Quality in Closed Loop

- ▶ Corrosion
- ▶ Scale formation & Fouling
- ▶ Total suspended solids (TSS)



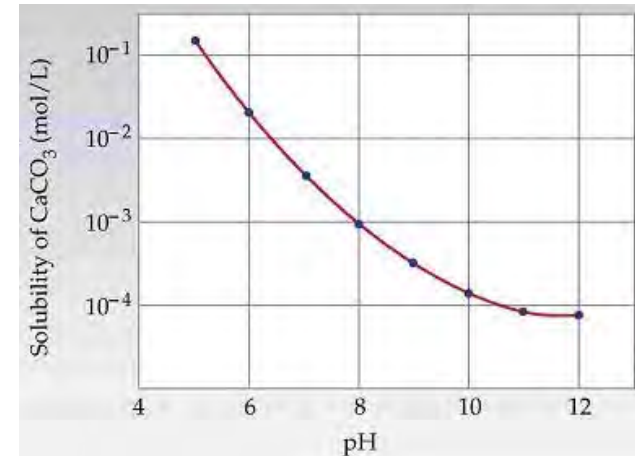
Water Quality – Corrosion

- ▶ High sulfur coals can produce low pH (4 – 6)
- ▶ Low sulfur coals tend to produce high pH (10 – 12)
- ▶ Largely depends on how much makeup water is added to system
- ▶ Wet/dry interfaces most susceptible
 - Overflow weirs and trough
 - Dewatering incline
- ▶ Acid or caustic injection can be used



Water Quality – Scale Formation

- ▶ Common with sub-bituminous coals
 - Usually calcium carbonate or aluminum hydroxide
- ▶ Factors affecting scale formation
 - Dissolved solids concentration
 - Concentration increases with water recirculation
 - pH
 - CaCO_3 precipitates at high pH
 - Sub-bituminous slurry samples pH = 10 – 12
 - Temperature
 - CaCO_3 solubility decreases at higher temperature (more dissolved solids precipitate as scale)
 - Closed loop systems will run a little higher water temperature (90 – 110 F)
 - Fouling due to deposition of suspended solids
 - High suspended solids increase scale potential by increasing number of nucleation sites



<http://www.ldeo.columbia.edu/~sanpisa/OceanSed%20project/class%20project/cac03phsol.JPG>

Water Quality – Scale Formation

▶ Controlling scale formation

- pH adjustment
 - Keep pH below critical value for precipitation
 - Not always successful long-term due to continual buildup of dissolved solids
- Scale inhibitors
 - Polymers attach to crystals to inhibit growth



Water Quality – Suspended Solids

- ▶ Impact of overflow TSS
 - Erosive wear
 - Pumps
 - Nozzles
 - Sludge accumulation
 - Seal water troughs
 - Refractory cooling pipes
 - Surge tanks
 - Fouling
 - Pipes
 - Pump intakes



Water Clarification – Extensive Lab Testing

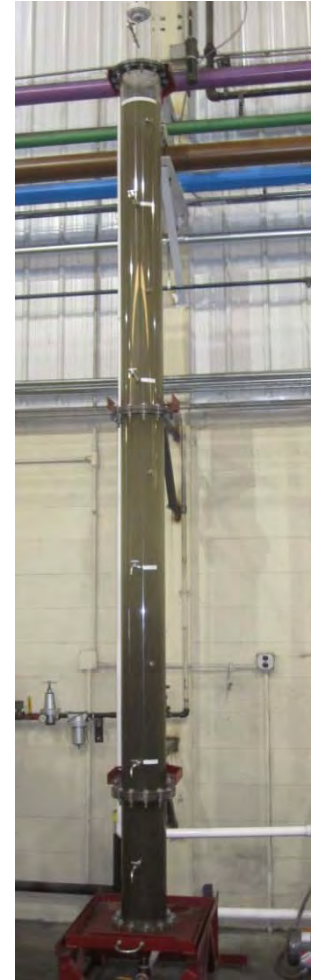
Lamella Clarifier Scale Model



RSC²™ Scale Model



Hydrobin/Settling Tank Scale Model



Settling Column



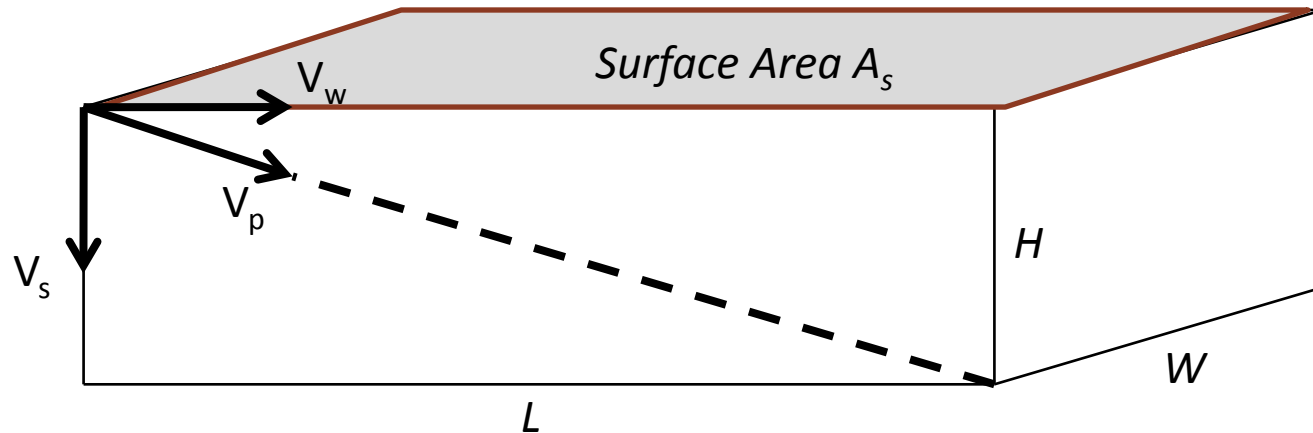
RSC²™ Module Approach

- ▶ Base RSC²™ can be configured with additional features to improve water quality
 - Longer settling section
 - 800 – 1000 ppm practical limit
 - Lamella plates
 - 200 – 400 ppm practical limit



RSCC with Lamella Plates

Longer Settling Section Clarification for Horizontal Flow



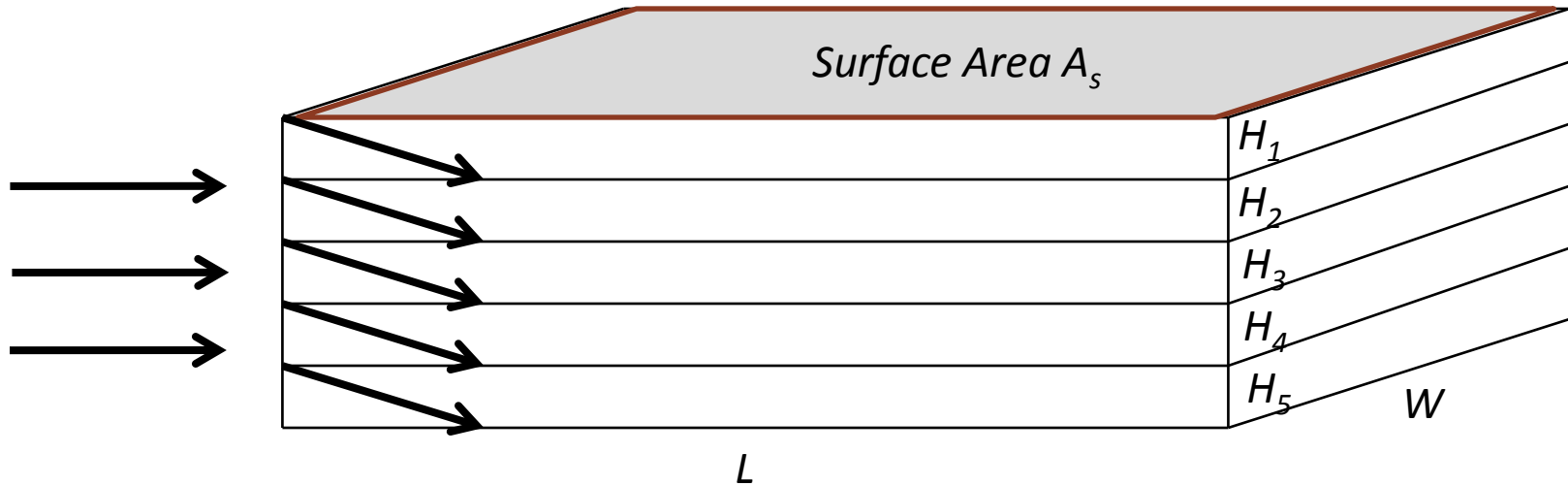
*For a particle starting at the top of the tank to settle,
Settling Time < Water Detention Time*

$$\text{Settling Time} = \frac{H}{V_s}$$

$$\text{Water Detention Time} = \frac{H * W * L}{Q}$$

$$\frac{H}{V_s} < \frac{H * W * L}{Q} \quad \text{simplifying,} \quad \frac{Q}{A_s} < V_s \quad \text{where} \quad V_s = \frac{d_p^2 (\rho_s - \rho_w) g}{18\mu}$$

Lamella Plates



*For a particle starting at the top of the tank to settle,
Settling Time \leq Water Detention Time*

$$\text{Settling Time} = \frac{H_1}{V_s} = \frac{1/5 H_{TOTAL}}{V_s}$$

$$\text{Water Detention Time} = \frac{H_{TOTAL} * W * L}{Q}$$

$$\frac{1/5 H_{TOTAL}}{V_s} \leq \frac{H_{TOTAL} * W * L}{Q}$$

simplifying,

$$\frac{Q}{A_s} \leq 5 * V_s$$



Summary

- ▶ RSC²[™] complies with ELG for bottom ash transport water by cleaning up water for reuse in closed loop
- ▶ Consider system water balance and need for draining tanks for maintenance
- ▶ RSC²[™] can be configured to provide advanced water treatment
 - Allows use of ash transport water as makeup to FGD
 - Provides flexibility to treat miscellaneous plant wastewater
 - Equipment washdown water
 - Consider isolating such water from ash transport water by using extra or spare RSC²[™]

B&W



THANK YOU